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## Formations of polyvinyltoluene microlatexes in quaternary oil in water cetyltrimethylammonium bromide microemulsions

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**Abstract** Polymerization of vinyltoluene (VT) in quaternary microemulsions containing cetyltrimethylammonium bromide (CTAB) as the cationic surfactant is studied using laser Raman spectroscopy (LRS) and dilatometry. The influences of water soluble (potassium peroxodisulphate, ammonium peroxodisulphate) and oil soluble (azobisisobutyronitrile, benzoyl peroxide) initiators, monomer, surfactant, cosurfactants (*n*-alcohol and bifunctional alcohols) and temperature on the rates of polymerization ( $R_p$ ), energy of activation ( $E_a$ ), particle diameter ( $D$ ), number of polymer particles ( $N_p$ ), molecular weight of polyvinyltoluene ( $\bar{M}_v$ ) and number of polymer chains per latex particle ( $N_{pc}$ ) are investigated. The dependencies of the kinetic and latex size parameters on the initiators and

cosurfactants are discussed in terms of the efficiency of the initiators in initiating the polymerization and on the interfacial partitioning behavior of various cosurfactants. The polymerization mechanism seems to follow Smith Ewart Case II hypothesis with two distinct rate regions. Final polymer microlatexes are found to lie within 10–50 nm as observed by transmission electron microscopy (TEM). Molecular weights are in the range of  $(1 \text{ to } 5) \times 10^6$ . Each latex particle contains one to three polymer chains.

**Key words** Vinyltoluene polymerization – microemulsion polymerization – dilatometry – laser Raman spectroscopy – polymer microlatexes – transmission electron microscopy – interfacial partitioning

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### Introduction

Production of stable monodisperse microemulsion ( $\mu$ E) suspensions of homopolymer microlatexes is a subject of current interest [1–2]. Size, stability and utility of the microlatexes may be controlled through the microstructure of  $\mu$ E droplets [1–3]. Among vinyl monomers, styrene and methylmethacrylate o/w  $\mu$ Es polymerizations are extensively investigated. A few reports on alkyl ring substituted styrene like vinyltoluene (VT) exist only for emulsion polymerization systems [13]. Methyl substitu-

tion (+*I* effect) renders greater resonance stability of the propagating radicals which lowers the rate of polymerization ( $R_p$ ) in the emulsion medium [13]. Since  $\mu$ Es serve as a media for enhanced rates [14] VT –  $\mu$ E polymerization would be an interesting case study.

Recently, VT-sodium dodecylsulphate (SDS) o/w  $\mu$ E polymerization with enhanced  $R_p$  compared to emulsion and bulk with nearly monodisperse latexes of high molecular weight ( $\bar{M}_v$ ) have been verified [15–17]. When SDS is replaced by cetyltrimethylammonium bromide (CTAB), the positively charged droplet interfaces may be expected to alter  $R_p$ , monomer and cosurfactant (CS) interfacial

partitioning, and the stability of the  $\mu$ Es. If initiators ( $I$ ) like potassiumperoxodisulphate (KPS) and ammoniumperoxodisulphate (APS) are used, the presence of positively charged micelle interfaces may create an attraction on the  $\text{SO}_4^-$  produced by the decomposition of the initiators in the water phase and thereby alter  $R_p$  values. In the present study, investigations on VT-CTAB  $\mu$ E polymerization and influences of  $I$ , CS, CTAB, VT and temperature on kinetic parameters, particle size and  $\bar{M}_v$  of the polymer are studied. Laser Raman spectroscopy (LRS) and dilatometry are utilized to monitor the kinetics of polymerization. Transmission electron microscopy (TEM) and viscosity average molecular weights ( $\bar{M}_v$ ) are used to characterize the final microlatexes.

## Experimental section

VT from Fluka was vacuum distilled under reduced pressure. CTAB from Sd.Fine, India was recrystallized from methanol mixture. *n*-Propanol (PrOH), *n*-butanol (BuOH), *n*-pentanol (PeOH), butylcarbitol (BuCa), carbitol (Ca), ethylcellosolve (ECe) and butylcellosolve (BuCe) from Sd.Fine, India, were distilled under reduced pressure. Recrystallized samples of azobisisobutyro nitrile (AIBN) and benzoyl peroxide (BP) (Kodak Chemicals, India) and APS and KPS (Aldrich) were used. Triple distilled water was used for all experiments. The o/w  $\mu$ Es region ( $L_1$ ) at 30 °C was determined by titrating the mixture of VT, water and CTAB with CS until transparency. All  $\mu$ Es were sealed, thermostated and  $\text{N}_2$  purged for about 40 min for replacement of air/ $\text{O}_2$  before their use in dilatometry and LRS. At 70 °C, hydroquinone was added to VT to inhibit thermal polymerization.

The LRS spectra were obtained with a Cary Model 82 laser Raman spectrometer with a Coherent Innova-70 Argon Laser (4880 Å) as the source following an earlier reported procedure [16]. Polymerization by dilatometry was carried out in a 20 ml capacity double-walled dilatometer assembly through which thermostated water was circulated and fitted with a 40-cm-long capillary (i.d. 1 mm). Calibration of the capillary height with conversion curves was made by gravimetric method. The slopes of the percentage conversion-time plots were used for  $R_p$  determinations.

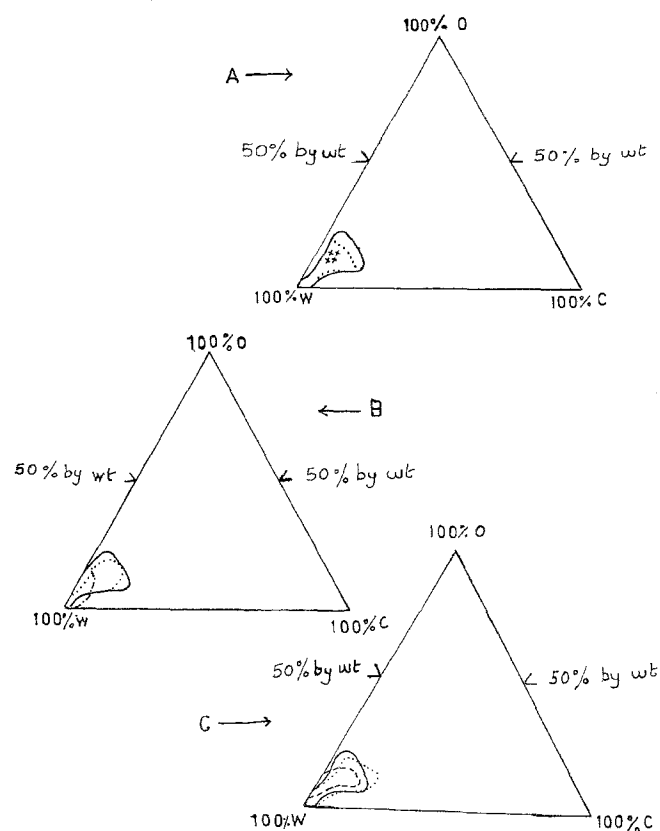
One drop of polymerized latex was added to 2 ml of 2% phosphotungstic acid solution and one drop of this mixture was put on a Formvar-coated copper grid of 400 mesh and photos were taken using a Philips 400 Transmission Electron Microscope. The particle diameter ( $D$ ) was measured by the Zeiss MOP-3 Analyser. The polymerized  $\mu$ E latexes were precipitated in excess of methanol and washed with excess methanol to remove CTAB and dried

in vacuum at 45 °C.  $\bar{M}_v$  of the polymer was determined at 30 °C by Ubbelohde dilution viscometer.

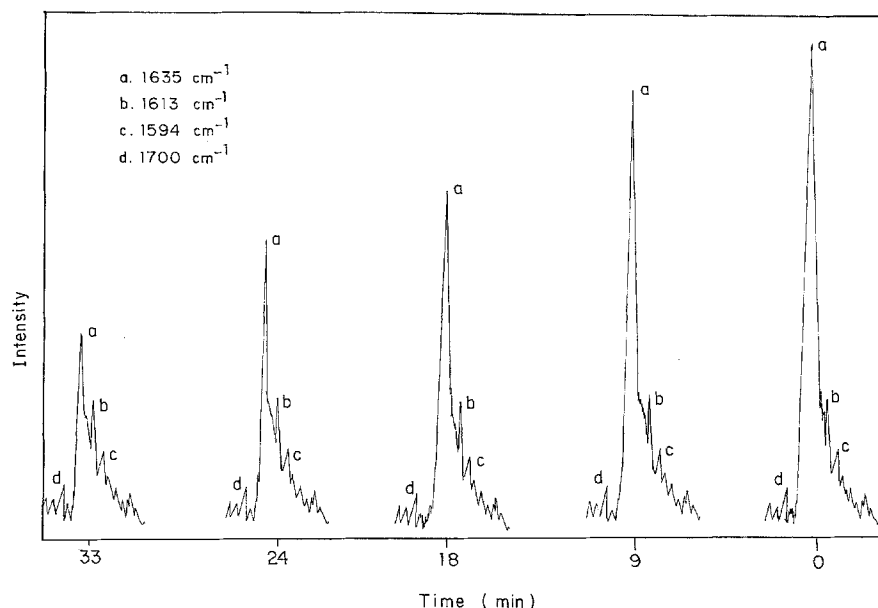
## Results and discussion

Monophasic  $\mu$ Es from water corner and extending towards oil corner at 30 °C is similar but slightly greater than at 70 °C (Fig. 1A). This is due to the temperature-dependent  $\mu$ E droplet breakdown leading to phase separations. Beyond the phase boundaries, bicontinuous and oil-rich regions ensue. Due to the hydrophilic nature of BuCa and interfacial partitioning of VT, the monophasic regions are found to be larger in area for these systems as compared to other CSs (Fig. 1B). For a fixed ratio of BuCa/CTAB (1.12), maximum solubilization of VT upto 12% is obtained. Increase in CTAB increases the  $\mu$ E region near water corner (Fig. 1C). At fixed weight proportions of VT, BuCa and water, an increase in CTAB/VT ratio above 0.8 results in the single phase  $\mu$ Es becoming more translucent.

**Fig. 1** Partial pseudoternary phase diagrams (wt %) of vinyltoluene (VT)-CTAB (C)-water (W)-alcohol microemulsions.  $\circ$  = VT + alcohol;  $\star$  denote compositions utilized for polymerization. **A**  $\circ$  = VT + BuCa; (—) 30 °C; ( $\times \times$ ) 70 °C **B** At 30 °C  $\circ$  = VT + BuCa (—); VT + BuCe ( $\cdots$ ); VT + PeOH ( $- \cdot -$ ) **C** At 30 °C;  $\circ$  = VT + BuCa; C = 0.274 M (—); 0.206 M ( $\cdots$ ); 0.137 M ( $- \cdot -$ )



**Fig. 2** A typical LRS variation of C=C peak intensity with time for vinyltoluene-CTAB microemulsions at 70 °C. [KPS] = 1.0 mM; [CTAB] = 0.207 M; [VT] = 0.57 M

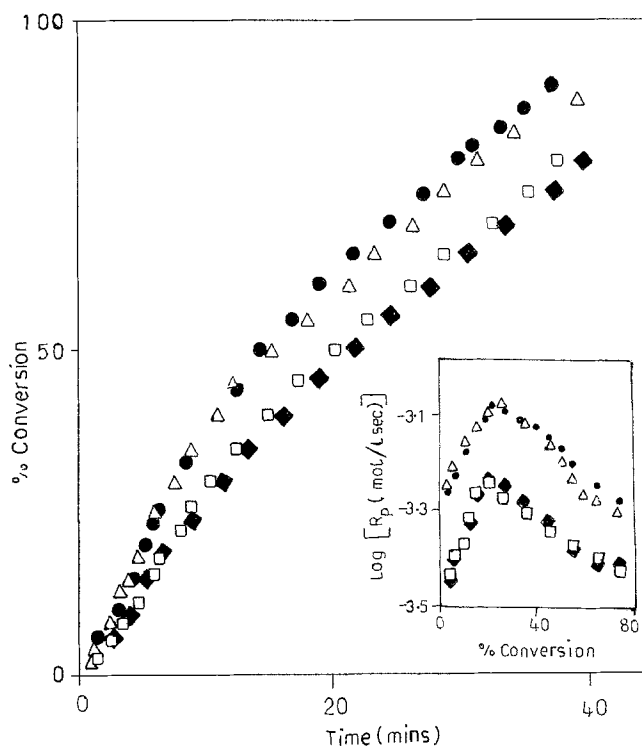


When this ratio exceeds 1.5, a highly viscous, bluish and flaky surfactant-rich phase is obtained.

The LRS intensity variation of C=C peak ( $1635\text{ cm}^{-1}$ ) of the monomer with time was used to evaluate  $R_p$ . A linear relationship between the monomer concentration and integral area of the peak was observed in agreement with earlier reports [8, 16]. The base peaks B, C and D (Fig. 2) do not pertain to vinyl group. The dilatometric and LRS measurements concur with each other. The values of the rate of polymerization obtained for 5% conversions are considered as  $R_{pi}$  values.

Two stages of polymerization rates occur in the present system (Fig. 3). In Step I, the rate increases due to the increase in the number of the nucleation loci and reaches a maximum ( $R_{pmax}$ ) when all the noninitiated monomer swollen droplets have disappeared by diffusion of the monomer to the growing particles. In Step II, due to the consumption of the monomer within the growing polymer particles, the rate decreases (Fig. 3). Such two-stage intervals have been reported earlier in  $\mu$ Es [4, 7]. For APS and KPS systems the kinetic values are identical. Hence KPS system is considered for discussion.  $R_{pmax}$  is achieved at 15–20% for AIBN and BP while for KPS and APS at 20–25% conversions.

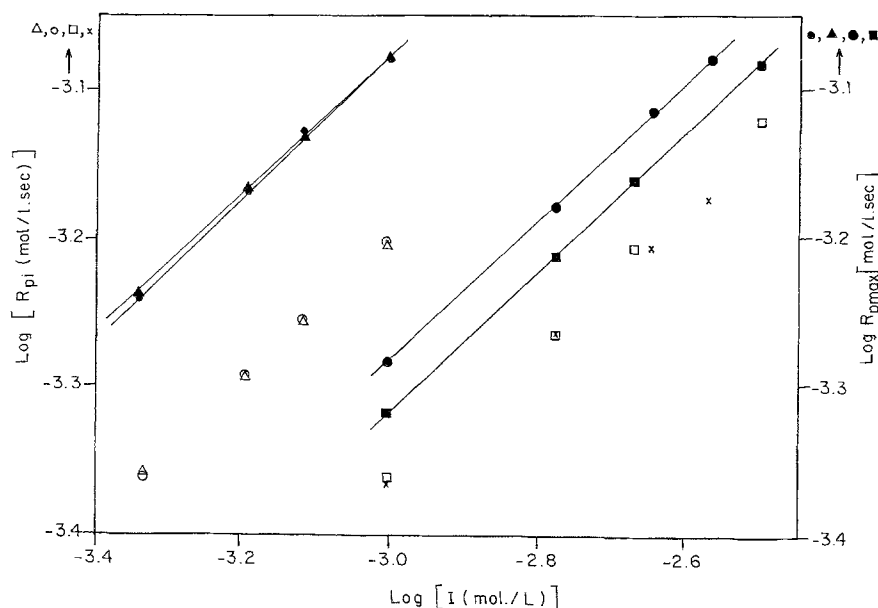
Longer  $I_p$  values and slightly lower rate values are obtained in CTAB-VT  $\mu$ Es compared to the SDS-VT  $\mu$ Es reported earlier [16]. This may be due to the attraction of the  $\text{SO}_4^-$  radicals on the CTAB droplet interfaces, which lengthens the residence time of the primary radicals on the droplet interface. This increases  $I_p$  (Fig. 6) and decreases  $R_{pi}$  (Fig. 4).  $R_{pi}$ ,  $\bar{M}_v$  and number of polymer particles ( $N_p$ ) dependency powers of KPS, AIBN, BP vary slightly while  $R_{pmax}$  dependencies are invariant (Table 1).



**Fig. 3** Percentage conversion versus time plots for 1.0 mM initiator concentrations at 70 °C. [VT] = 0.57 M; [CTAB] = 0.206 M. (Δ) KPS; (●) APS; (◆) AIBN; (□) BP. Inset: Log  $R_p$  versus conversion for the system of composition as in Fig. 3. (Δ) KPS; (●) APS; (◆) AIBN; (□) BP

Based on the decomposition rate constants ( $k_d$ ) of the  $I$  [18a] the radical generation rates of 1.0 mM KPS, AIBN and BP are  $4.66 \times 10^{-8}$ ,  $7.6 \times 10^{-8}$  and  $3.66 \times 10^{-8}$  mol/L.s respectively, indicating that concentration of

**Fig. 4** Variation of  $\log R_{pi}$  and  $\log R_{pmax}$  (filled symbols) with initiator concentrations. ( $\circ$ ,  $\bullet$ ) KPS; ( $\Delta$ ,  $\blacktriangle$ ) APS, ( $\square$ ,  $\blacksquare$ ) AIBN; ( $\times$ ,  $\bullet$ ) BP



primary radicals fall in the order AIBN > KPS > BP. Hence, in case of BP, lower values of  $R_{pi}$  (Fig. 4) and higher  $I_p$  values than KPS (Fig. 6) and AIBN (Fig. 7) are seen. In case of AIBN, decomposition produces uncharged cyanoisopropyl radicals which can diffuse out of the droplet to the aqueous phase. This lowers the AIBN efficiency ( $R_{pi}$  low) (Fig. 4). For the AIBN and BP systems the initiation in the droplets is limited by droplet volume, viscosity increase (cage effect), desorption and subsequent terminations of the radicals. These processes reduce the efficiency of the radicals. The reentry of the desorbed radicals may also contribute to droplet nucleations. Similar effects of desorption and reentry on emulsion polymerization has been well described by Nomura's theory [19]. For all initiators  $R_{pi}$  values increase with  $I$  since droplet initiations and number of nucleated droplets in  $\mu E$  increase proportionately with  $I$ . The propagating loci attains a maximum rate depending upon the droplet monomer composition and remains invariant towards  $I$  type. Hence a constant dependency of  $R_{pmax}$  on  $[I]$  for all initiators is observed (Table 1).

$\bar{M}_v$  values exhibit a decreasing trend with increasing  $[I]$ , due to the increasing number of chain terminations. From the TEM photos of the polymer microlatexes (Fig. 5), the mean volume diameter ( $D$ ) and  $N_p$  values are noted.  $N_p$  values increases with  $[I]$ , since the number density of the nucleated droplets increase with  $[I]$  (Figs. 6 and 7). Decrease in  $D$  values with  $[I]$  is due to the lesser availability of propagating monomers as well as increase in radical termination steps. Hydrophobic initiators (AIBN, BP) seem to produce particles with higher  $D$  values (Fig. 7) than hydrophilic KPS and APS systems (Fig. 6).

**Table 1** Kinetic parameters of vinyltoluene-water-CTAB-butylcarbitol o/w microemulsion polymerizations

Initiator	$R_{pi}^a$	$R_{pmax}^a$	VT <sup>b</sup>	$N_p^a$	$R_{pi}^c$	$I_p^c$
KPS	0.48	0.48	1.20	0.37	0.05	0.22
APS	0.46	0.47	1.16	0.37	0.05	0.23
AIBN	0.48	0.49	1.04	0.37	0.01	0.06
BP	0.46	0.49	1.09	0.38	0.01	0.07

The values given in the table are slopes of log-log plots.

<sup>a</sup>  $\log R_{pi}$ ,  $\log R_{pmax}$  and  $\log N_p$  versus  $\log [I]$ .

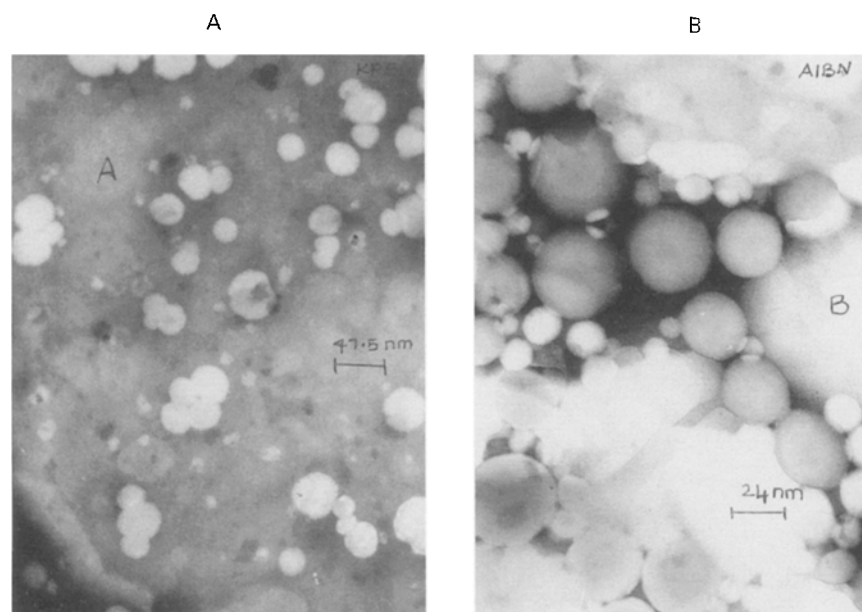
<sup>b</sup>  $\log R_{pmax}$  versus  $\log [VT]$  in presence of various initiators.

<sup>c</sup>  $\log R_{pi}$  and  $\log I_p$  versus  $\log [CTAB]$ .

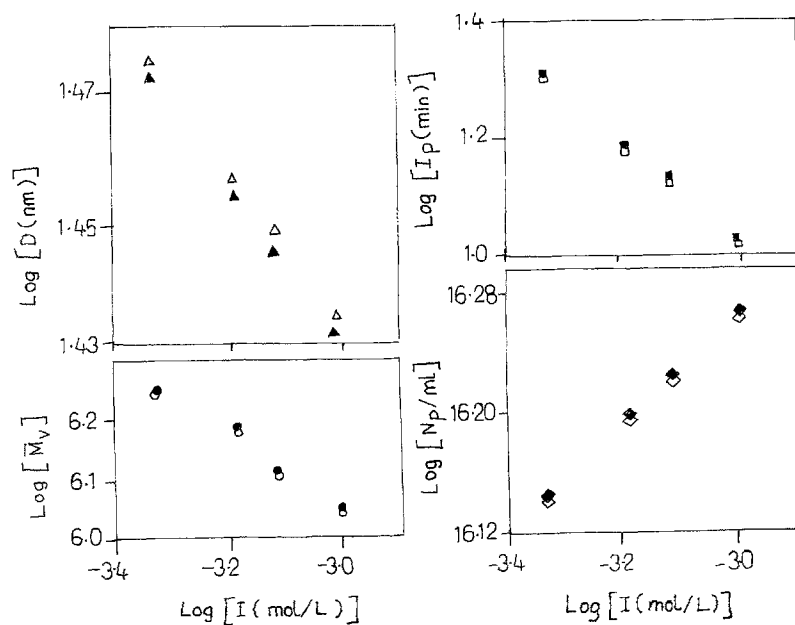
$N_p$  depends on the number density of the nucleated droplets and on  $[I]$  (Figs. 6 and 7). High values of  $\bar{M}_v$  and low values of  $N_{pc}$  (2–3 polymer chains per droplet) indicate that contribution to mechanism of chain deactivation is mainly from the interfacial chain transfer of the free radicals which is one of the mode of desorption of radicals. With increase in  $[I]$  the % yield increases. The dependency of  $R_{pmax}$  and  $N_p$  on  $[I]$  is quite consistent with the prediction of 0.48 and 0.4 by Smith Ewart Case II hypothesis and hence the same mechanism may be envisaged here.  $R_{pmax}$  and  $D$  values at lower [KPS] equal those at higher [AIBN] and [BP]. In KPS systems initiator radicals are available to all droplets for initiation. Thus a single KPS radical is equivalent to 1–3 radicals of BP and 3–5 radicals of AIBN in nucleating a droplet. This makes KPS/APS more efficient than AIBN and BP (Table 2).

Toluene and dodecane are used as diluents to study monomer effect. For all  $I$ ,  $R_{pi}$  and  $\bar{M}_v$  increases with  $[VT]$

**Fig. 5** TEM photographs of polyvinyltoluene microlatex obtained from vinyltoluene - CTAB-BuCa- water micro-emulsion polymerization initiated by **A** KPS and **B** AIBN



**Fig. 6** Variation of  $\log I_p$ ,  $\log \bar{M}_v$ ,  $\log D$  and  $\log N_p$  with KPS (filled symbols) and APS (open symbols) concentrations

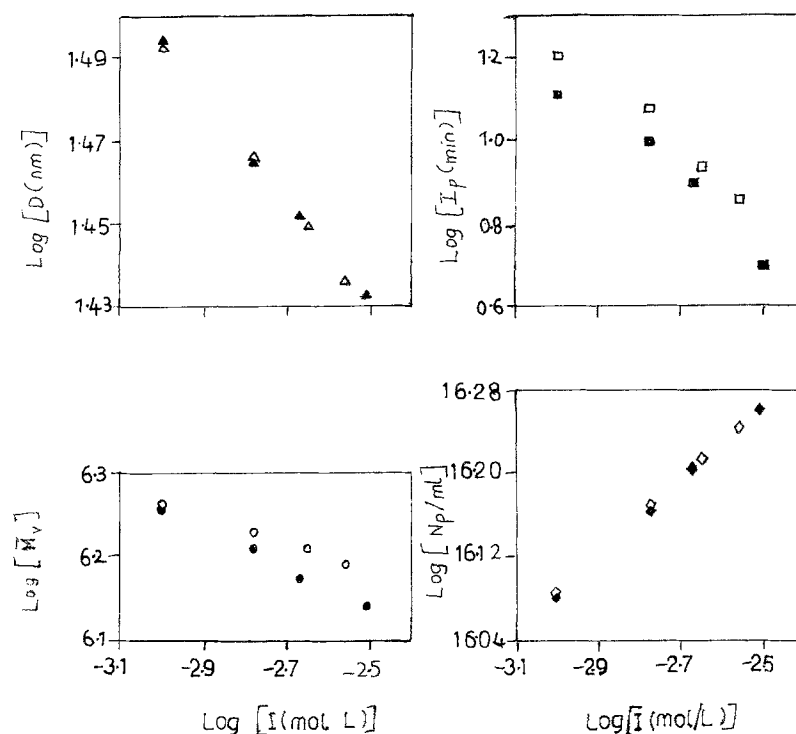


at constant CTAB due to increased availability of the monomer within each droplet. Due to increase in chain transfers to the solvent, rate dependencies greater than 1 are obtained. Since  $[CTAB]$  is greater than CMC the number density of the oil swollen droplets is greater than the number of free radicals generated and the number density of the droplets which deplete during polymerization. Hence  $R_p$  and  $\bar{M}_v$  values remain unaltered. However the  $I_p$  values of persulphate initiators show a greater

dependency on  $[CTAB]$  than AIBN and BP due to the positive interface and  $SO_4^-$  radicals interaction (Table 1). Increase in  $[CTAB]$ , increases the number density of the droplets consequently decreasing the particle size (Fig. 8).

For all  $I$ , the cosurfactant (CS) effect on the dependency parameters remains the same (Table 3). Variations are observed due to differences in chain transfers to the CSs. Unlike bifunctional CSs,  $R_{pi}$  remains invariant in monofunctional CSs. Due to enhanced solubilization of

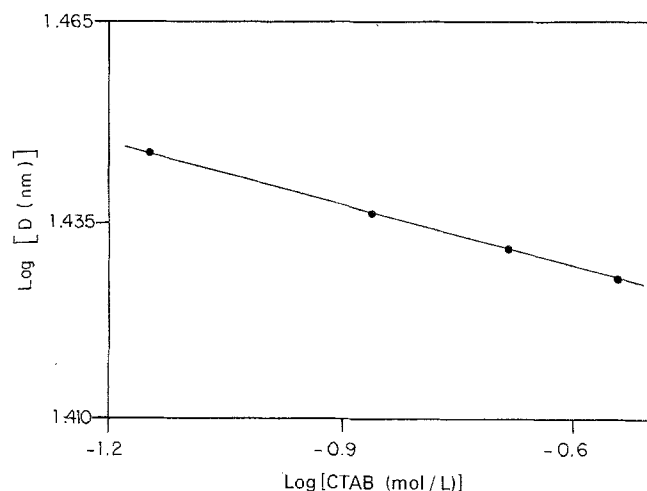
**Fig. 7** Variation of  $\log I_p$ ,  $\log \bar{M}_v$ ,  $\log D$  and  $\log N_p$  with AIBN (filled symbols) and BP (open symbols) concentrations



**Table 2** Similar polymer microlatex features of o/w vinyltoluene microemulsion polymerizations. System considered water (82.4%); vinyltoluene (5.5%); butylcarbitol (5.9%); CTAB (6.2%)

Features	Initiator Types		
	KPS	AIBN	BP
Concn. (mM/L)	1.00	3.13	2.67
$R_{pmax}$ ( $10^{-4}$ mol/L.sec)	8.33	8.29	8.34
$D$ (nm)	27.0	27.1	27.3
$N_p$ ( $10^{15}$ /ml)	18.6	18.4	17.6
Rate of free radical generation ( $10^{-8}$ mol/L.sec)	4.66	23.7	9.77
1 KPS radical equivalent to	—	5.0	2.1

VT by bifunctional CSs, larger latexes are obtained with bifunctional CSs. From the known chain transfer constants of a few alcohols [18b], it can be observed that chain transfer is not much affected by CS type. Hence the variation in  $\bar{M}_v$  in presence of various CSs can be effectively attributed to difference in CS interfacial partitionings and the influences on the termination processes. The overall activation energy ( $E_a$ ) is found as 12–22 Kcals/mol. Unlike SDS- $\mu$ Es [16] wherein  $E_a$  is independent of type of initiator.  $E_a$  is slightly higher for KPS/APS-CTAB  $\mu$ Es (21.6 Kcals/mol) than AIBN (13.5 Kcals/mol) and BP  $\mu$ Es (13.0 Kcals/mol). Since the decomposition energies of the initiators are comparable [18] the  $E_a$  difference is due to the increased energy barrier caused by the positive



**Fig. 8** Variation of particle diameter ( $D$ ) (●) with CTAB concentrations [KPS] = 1.0 mM; [VT] = 0.5 M

droplet interface over  $SO_4^-$  radicals.  $E_a$  is dependent on the CS type due to the increase in the interfacial partitioning, fluidity and curvature of the interfaces that consequently alters the potential barrier for initiation and other subsequent steps.  $R_{pmax}$  values are found to be 3–4 times greater than styrene counterpart [7]. In VT, the methyl group of the aromatic ring seems to cause greater stabilization of the propagating radicals through the

**Table 3** Kinetic parameters of vinyltoluene-CTAB, o/w microemulsion polymerization with different cosurfactants [VT] = 0.57 M; [KPS] = 0.47 mM; [CTAB] = 0.207 M

CS	[KPS] <sup>a</sup>	[VT] <sup>b</sup>	Ea Kcals/mol	$\bar{M}_v \times 10^6$	D nm
BuCa	0.48	1.20	21.6	1.79	29.7
Ca	0.44	1.17	20.98	1.70	28.8
BCe	0.48	1.2	20.2	1.53	28.3
Ce	0.45	1.18	19.23	1.40	27.3
PeOH	0.41	1.10	18.28	1.51	26.0
BuOH	0.39	1.22	15.38	1.24	25.1
PrOH	0.39	1.24	13.54	1.09	23.7

<sup>a</sup> The values are slopes of  $\log R_{pmax}$  versus  $\log[KPS]$  plots.<sup>b</sup> The values are slopes of  $\log R_{pmax}$  versus  $\log[VT]$  plots.

hyperconjugation effect. The methyl group of the aromatic ring seems to cause greater stabilization of free radicals and more residence time of radicals.

## Conclusions

In VT polymerization aided by CTAB, KPS is found to be a more efficient *I* than AIBN and BP. BuCa, as the CS seems to produce higher dependencies of kinetic parameters with *[I]*. Lower *Ea* values are seen for propanol-containing microemulsions. On comparing SDS-VT  $\mu$ Es, *I<sub>p</sub>* and *Ea* values are increased in the presence of hydrophilic initiators. This is due to the electrostatic interaction of positive CTAB droplet interface with  $SO_4^-$  radicals. Higher *R<sub>pmax</sub>* values seen for VT  $\mu$ E polymerization than for styrene  $\mu$ E polymerization is due to the methyl substitution in the aromatic ring.

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